

## Electrolytic Carbons from CO<sub>2</sub> and Their Applications

Ping Peng,<sup>1</sup> Ao Yu,<sup>1</sup> Jiawen Ren<sup>2\*</sup> and Fangfang Li<sup>1\*</sup>

Tremendous efforts have been paid to tackle our energy crisis and environmental issues. CO<sub>2</sub> as main source for the greenhouse effect, is very abundant in nature and can be used as feedstock to prepare value-added carbon materials via electrochemical reduction. By carefully manipulating electrolysis current density, electrolyte composition, electrode materials and temperature, various functional carbon materials, including carbon nanotubes (CNTs), graphene, graphite, nanodiamonds, etc., could be readily generated with high Faraday Efficiency. As-obtained materials exhibits excellent performances in energy applications like batteries and supercapacitors. Electrochemical reduction of CO<sub>2</sub> provides a promising pathway for CO<sub>2</sub> capture and conversion and creates materials suitable for high energy power/density devices.

**Keywords:** CO<sub>2</sub> reduction; Carbon nano-structures; Molten salt; Electrolytic

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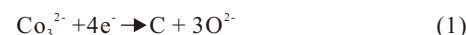
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### 1. Introduction

The rising levels of atmospheric carbon dioxide, predominantly because of anthropogenic activities such as fossil fuel burning,<sup>1</sup> is threatening the sustainable development of the society. The globe climate change, mainly due to the increased CO<sub>2</sub> concentration,<sup>2</sup> has attracted plenty of attention to develop technologies that can achieve a reduction of atmospheric CO<sub>2</sub> to a sustainable level. Despite of the fact that plants can absorb CO<sub>2</sub> by photosynthesis process,<sup>3</sup> the decrease of CO<sub>2</sub> level is still impossible by plants compared to the high speed of population increase and expanded industry. Many efforts have been made on the capture of carbon dioxide and conversion into CO,<sup>4,6</sup> formic acid,<sup>7</sup> alcohols,<sup>8-10</sup> and hydrocarbons,<sup>11-13</sup> methane<sup>14</sup> by a chemical way, such as hydrogenation reaction. In these conversion processes, CO<sub>2</sub> acts as the chemical feedstock for the manufacturing of valuable chemicals, however, these routes for CO<sub>2</sub> conversion are bottle-necked by the cost, such as expensive catalysts, which hinders the development of these methods.

In contrast, liquid-phase electrochemical reduction of CO<sub>2</sub> into useful chemicals has been widely studied and reviewed recently by Paul. J Kenis<sup>15</sup> and Jiujun Zhang.<sup>16</sup> The standard reduction potential of CO<sub>2</sub> is very close to hydrogen evolution but it has a low solubility in aqueous solution. Thus, in many cases, hydrogen evolution is predominant. The low Faraday efficiency as well as further gas separation makes this process still far away from commercialization.

Room temperature ionic liquids (RTILs) with wide electrochemical window and high solubility of CO<sub>2</sub> have been studied for CO<sub>2</sub> reduction, but the high cost and toxicity of RTILs hamper their further commercial applications.<sup>11,17,18</sup> In contrast to these electrolytes, molten salts render low cost, low toxicity and high ionic conductivity with a low vapor pressure, and have been proven as practical electrolytes for capture and electrochemical reduction/splitting of CO<sub>2</sub>.<sup>19</sup> This method relies on the reduction of dissolved CO<sub>2</sub> between two biased electrodes, where either solid carbon, generally formed below 850 °C, or CO, when >950 °C, is deposited at the cathode, with very high coulombic efficiency.<sup>20,21</sup> In temperature between, carbon and CO are co-synthesized at cathode. The reaction at cathode is either Eq. (1) or Eq. (2). However, it should be noted that carbon could be generated by direct electrolysis of CO<sub>2</sub> either at room temperature or melting salts, but high pressure is required in both cases.<sup>22</sup> The reaction is as listed in Eq. (3)



The deposited carbons at cathodes, initially, were not received much attention. The discovery of fullerenes,<sup>23,24</sup> CNTs,<sup>25</sup> and graphene,<sup>26,27</sup> ignited tremendous interests on nano-carbons because of their unique features in electronics, mechanics, chemical properties and supramolecular chemistry.<sup>28,29</sup> These also put questions to the researchers on the possibility of generating such nano-carbons by electrolysis of CO<sub>2</sub> or carbonates. The recent efforts clearly demonstrated that nanocarbons like nanotubes,<sup>30-33</sup> nanofibers,<sup>34</sup> graphene,<sup>35</sup> nanodiamond,<sup>36-38</sup> nanographite<sup>39</sup> and hollow spheres<sup>40</sup> could be generated by direct or indirect reduction of carbon dioxide. The advanced features of this methodology are (1) the carbon properties, such as size, shape, surface

<sup>1</sup>State Key Laboratory of Materials Processing and Die & Mould Technology, School of Materials Science and Engineering, Huazhong University of Science and Technology, Wuhan 430074, China

<sup>2</sup>Department of Chemistry, The George Washington University, Washington, DC 20052, USA

\*E-mail: ren.jiawen@gmail.com; fflf@hust.edu.cn

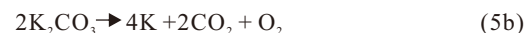
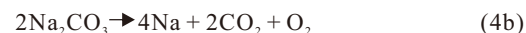
areas and defects could be tailored by the composition of electrolyte,<sup>41-44</sup> electrolysis temperature,<sup>45,46</sup> current density and the electrode materials,<sup>41,47</sup> a big variety of carbons could be produced;<sup>48</sup> (2) the B, S and P hetero-atoms could be in-situ doped simply by adding corresponding metal salts rather than to use organic or expensive chemicals as in wet-synthesis or gas-deposition method;<sup>51,48-50</sup> (3) the resulting materials have shown excellent performances in supercapacitors and batteries;<sup>51-56</sup> (4) the large-scale production is possible as indicated from prof. Licht's work,<sup>57</sup> promising technique for the CO<sub>2</sub> capture and conversions.

## 2. Thermodynamics of CO<sub>2</sub> reductions

As mentioned above, the electrochemical reduction of CO<sub>2</sub> at room temperature is relatively complicated, the products could be CO,<sup>58</sup> formate<sup>59</sup> or formic acid,<sup>60</sup> methanol,<sup>61</sup> or hydrocarbons,<sup>12</sup> depending on the electrolyte and catalysts used. The thermodynamic electrochemical half-reactions of CO<sub>2</sub> reduction and their associated standard electrode potentials are listed in Table 1.<sup>16</sup> It is worthy to mention that the reactions listed in Table 1 are thermodynamic, for aqueous solutions, giving indication of each reaction's tendency and possibility but no indicating the reaction's kinetics, such as rate and mechanism. Although the carbon deposition needs higher voltage ( $E^0 = 0.21$  V), meaning easier, than hydrogen evolution ( $E^0 = 0$  V) reaction, the kinetics problems make the later one is predominant in most cases. The studies to solve the problems of sluggish reduction rate, low selectivity (multi-products) and high overvoltage are on-going by many groups, mainly focusing on the production of hydrocarbons or methanol or CO, though pure carbon could be generated with high pressure of CO<sub>2</sub> in non-aqueous electrolyte, as shown in the next section.

In molten carbonates, the reactions happened also had a debate for a long time. Recent progress stepped further on the verification of the reactions. In most experiments, one of Li<sub>2</sub>CO<sub>3</sub>, Na<sub>2</sub>CO<sub>3</sub>, K<sub>2</sub>CO<sub>3</sub>, CaCO<sub>3</sub>, and BaCO<sub>3</sub>, or a mixture of above was involved and the reactions during electrolysis are directly dependent on the electrolyte used. In

pure Na<sub>2</sub>CO<sub>3</sub> or K<sub>2</sub>CO<sub>3</sub>, or corresponding mixture, results from several group suggested the metal was deposited, and the cathode would get burning whenever contact with air.<sup>62</sup> Based on these results, the reaction in this system probably is either Eq. (4) or (5).



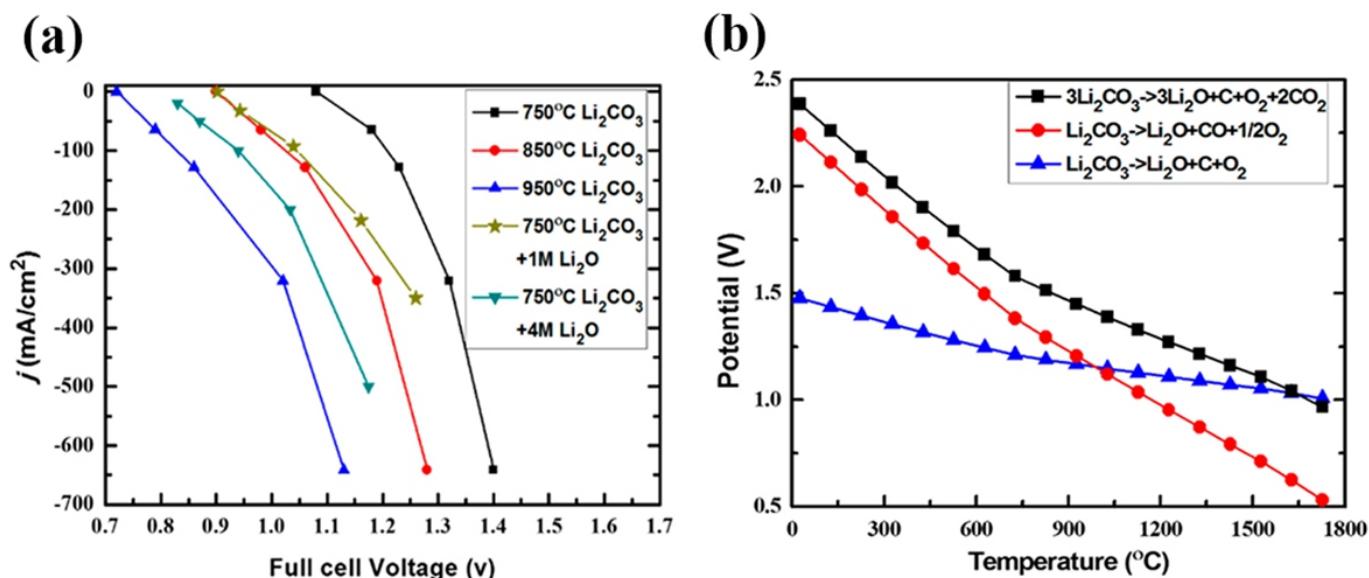
When CaCO<sub>3</sub> is the main component of an electrolyte, e.g., Ca/Ba, Ca/Na, Ca/K or Ca/Na/K carbonate, the main reaction supposed to be Eq. (6). The reason is that



CaO has a very limited solubility in the molten carbonates and would precipitate immediately after generation, which lead to a shortage of oxygen ions (O<sup>2-</sup>) at anode and therefore the reaction (7) is dominated at anode. This conclusion was further confirmed by our group's experiments.<sup>31</sup> Two experiments were conducted, one was



with pre-mixed carbonate electrolyte, containing CaCO<sub>3</sub> and Li<sub>2</sub>CO<sub>3</sub>, the other one was adding solid CaCO<sub>3</sub> into Li<sub>2</sub>CO<sub>3</sub> melt during electrolysis. CaO precipitated directly at cathode in the first experiment, while CaO precipitated at the bottom of the container in the second. This is because Ca<sup>2+</sup> ions distributed evenly in a pre-mixed electrolyte, while Ca<sup>2+</sup> ions mainly present around the CaCO<sub>3</sub> powder in the later experiment. The generated cathodic Li<sub>2</sub>O, which is high soluble in molten carbonates, diffused to anode and was captured by Ca<sup>2+</sup> ions and sedimented at the bottom of container. It should be noted that this conclusion is only



**Fig. 1** Experimental results vs thermodynamic calculations. (a) Experimental full cell potentials with Ir and steel as the anode and cathode, respectively; (b) Calculated standard potentials of carbon deposition or CO release reaction in pure Li<sub>2</sub>CO<sub>3</sub> electrolyte. Reprinted with permission from Ref. 64. Copyright 2015, American Chemical Society.

**Table 1** Selected standard potentials of CO<sub>2</sub> in aqueous solutions (V vs SHE) at 1.0 atm and 25 °C, calculated on the basis of the standard Gibbs energies of the reactants. Reprinted permission from ref. 16. Copyright 2014, Royal Society of Chemistry.

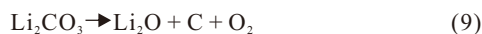
Half-electrochemical Thermodynamic reactions	Electrode potentials (V vs. SHE) under standard conditions
$\text{CO}_2(\text{g}) + 4\text{H}^+ + 4\text{e}^- = \text{C}(\text{s}) + 2\text{H}_2\text{O}(\text{l})$	0.210
$\text{CO}_2(\text{g}) + 2\text{H}_2\text{O}(\text{l}) + 4\text{e}^- = \text{C}(\text{s}) + 4\text{OH}^-$	-0.627
$\text{CO}_2(\text{g}) + 2\text{H}^+ + 2\text{e}^- = \text{HCOOH}(\text{l})$	-0.250
$\text{CO}_2(\text{g}) + 2\text{H}_2\text{O}(\text{l}) + 2\text{e}^- = \text{HCOO}^-(\text{aq}) + \text{OH}^-$	-0.1078
$\text{CO}_2(\text{g}) + 2\text{H}^+ + 2\text{e}^- = \text{CO}(\text{g}) + \text{H}_2\text{O}(\text{l})$	-0.106
$\text{CO}_2(\text{g}) + 2\text{H}_2\text{O}(\text{l}) + 2\text{e}^- = \text{CO}(\text{g}) + 2\text{OH}^-$	-0.934
$\text{CO}_2(\text{g}) + 4\text{H}^+ + 4\text{e}^- = \text{CH}_2\text{O}(\text{l}) + \text{H}_2\text{O}$	-0.070
$\text{CO}_2(\text{g}) + 3\text{H}_2\text{O}(\text{l}) + 4\text{e}^- = \text{CH}_2\text{O}(\text{l}) + 4\text{OH}^-$	-0.898
$\text{CO}_2(\text{g}) + 6\text{H}^+ + 6\text{e}^- = \text{CH}_3\text{OH}(\text{l}) + \text{H}_2\text{O}(\text{l})$	0.016
$\text{CO}_2(\text{g}) + 5\text{H}_2\text{O}(\text{l}) + 6\text{e}^- = \text{CH}_3\text{OH}(\text{l}) + 6\text{OH}^-$	-0.812
$\text{CO}_2(\text{g}) + 8\text{H}^+ + 8\text{e}^- = \text{CH}_4(\text{g}) + 2\text{H}_2\text{O}(\text{l})$	0.169
$\text{CO}_2(\text{g}) + 6\text{H}_2\text{O}(\text{l}) + 8\text{e}^- = \text{CH}_4(\text{g}) + 8\text{OH}^-$	-0.659
$2\text{CO}_2(\text{g}) + 2\text{H}^+ + 2\text{e}^- = \text{H}_2\text{C}_2\text{O}_4(\text{aq})$	-0.500
$2\text{CO}_2(\text{g}) + 2\text{e}^- = \text{C}_2\text{O}_4^{2-}(\text{aq})$	-0.590
$2\text{CO}_2(\text{g}) + 12\text{H}^+ + 12\text{e}^- = \text{CH}_2\text{CH}_2(\text{g}) + 4\text{H}_2\text{O}(\text{l})$	0.064
$2\text{CO}_2(\text{g}) + 8\text{H}_2\text{O}(\text{l}) + 12\text{e}^- = \text{CH}_2\text{CH}_2(\text{g}) + 12\text{OH}^-$	-0.764
$2\text{CO}_2(\text{g}) + 12\text{H}^+ + 12\text{e}^- = \text{CH}_2\text{CH}_2\text{OH}(\text{l}) + 3\text{H}_2\text{O}(\text{l})$	0.084
$2\text{CO}_2(\text{g}) + 9\text{H}_2\text{O}(\text{l}) + 12\text{e}^- = \text{CH}_2\text{CH}_2\text{OH}(\text{l}) + 12\text{OH}^-$	-0.744

applicable in molten carbonate, different mechanisms may be possible in other melts depending on the solubility of CaO.

On the other hand,  $\text{BaCO}_3$ , also an alkaline earth metal carbonate, exhibited different behavior.<sup>63</sup> In the electrolyte of Ba, Ba/Na, Ba/K or Ba/Na/K molten carbonates, the main reaction is (8) due to the good solubility of BaO. However, the electrolysis in pure  $\text{Li}_2\text{CO}_3$  or melts with  $\text{Li}_2\text{CO}_3$  is relatively complicated.



$\text{Li}_2\text{O}$  has a high solubility of up to 9 M/kg in  $\text{Li}_2\text{CO}_3$ . Thus, it is reasonable that the main reaction should be similar to Eq. (8), that is:



Unfortunately, the thermodynamic calculation results based on Eq. (9) (Fig. 1b) is much larger than the experimental results as shown in Fig. 1a.<sup>64</sup>

The presence of either  $\text{Li}_2\text{O}$  or  $\text{CO}_2$ , or increase the  $\text{CO}_2$  pressure can further reduce the reaction potential in pure  $\text{Li}_2\text{CO}_3$  electrolyte. The reaction was supposed by our group as Eq. (10).

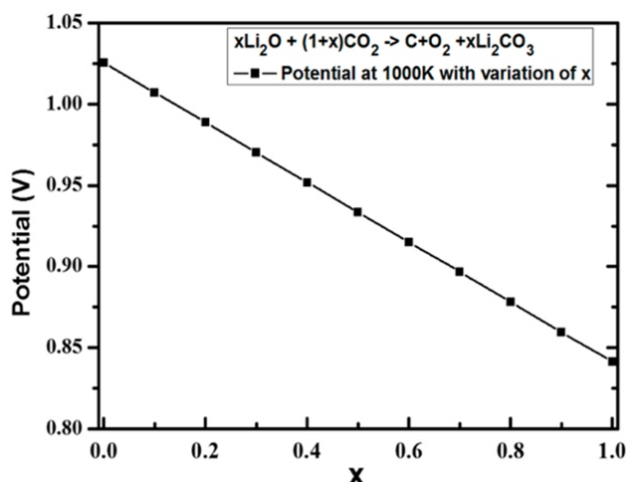


Fig. 2 Standard potentials of reaction (10) with variation of x. Reprinted with permission from Ref. 64. Copyright 2015, American Chemical Society.

Table 2 shows the calculated standard potentials of carbon deposition in different systems based on above reactions. The calculations are based on the Nernst Eq.  $\Delta G^0 = -nE^0F$ , where the  $\Delta G^0$ , n,  $E^0$ , and F represent standard Gibbs free energy change, number of transferred electrons, standard reaction potential, and Faraday constant, respectively.

Another feature of the carbon deposition from carbonate is that hetero-atoms could be incorporated simply by adding corresponding salt into the melts. Table 3 shows some calculated standard potentials for the reference of possible doping element.

### 3. Directly $\text{CO}_2$ splitting

Although the potential of  $\text{CO}_2$  splitting into carbon and oxygen is almost independent of temperature,  $\sim 1.02$  V, from thermodynamic calculations, it was difficult to reduce  $\text{CO}_2$  into carbon at room

temperature in aqueous solution because of side reactions. Using ionic liquid 1-n-butyl-3-methylimidazolium hexafluorophosphate ( $[\text{Bmim}]\text{PF}_6$ ) as the electrolyte and glassy carbon as the cathode, Lu *et al.*<sup>65</sup> carried out a series of studies on the electrochemical reduction of  $\text{CO}_2$  at 25–100 °C under various  $\text{CO}_2$  pressures (1–5 atm). The results show that the Faraday efficiency is directly related to the  $\text{CO}_2$  pressure, higher pressure, better efficiency. The more interesting part is that the resulted product at cathode is a mixture of “carbon-nanotubes” of  $\sim 33$  nm, nanographites, and amorphous carbons, as claimed by authors. However, it is still questionable that these “carbon-nanotubes” are tubular amorphous carbon or real carbon nanotubes due to the lack of further characterizations, e.g., Raman, TGA, etc. It may deserve to further study above results to confirm the product content, either in-situ products or after post-treatment of annealing.

Another study of direct  $\text{CO}_2$  splitting was performed by Inessa Novoselova *et al.*<sup>66</sup> at high temperatures. The electrochemical behavior of metal halide molten salts ( $\text{Na,K|Cl}$ ;  $\text{Na,K,Cs|Cl}$ ), saturated with  $\text{CO}_2$  under an excessive pressure of up to 1.5 MPa, has been investigated in the temperature range of 550–850 °C by cyclic voltammetry. An electrochemical-chemical-electrochemical (ECE) mechanism is proposed based on cyclic voltammetry (CV) results, and a mixture of carbon nano-particles of different forms and structures, e.g. crystalline graphite, blocks of amorphous carbon, carbon nanotubes (CNT) and nanofibers, were found at cathodic deposits. No estimation on the percentage of each is available in this report. The outer diameter of the tubes is 5–250 nm, and the internal diameter is 2–140 nm. One surprise is the existence of Fe (iron) in the deposits as shown in the XRD (Fig. 3c). This may be the reason of creation of CNTs as suggested by our reports<sup>31,32,57</sup> and chemical vapor deposition (CVD) methods.<sup>67,68</sup> The other interesting feature is that fullerene phase was detected when a halide melts of  $\text{Na,K,Cs|Cl}$  was used as the electrolyte. Further investigations may be needed to check out the possibility of synthesis of fullerene with high yield by  $\text{CO}_2$  reduction, either direct or indirect electrolysis carbonates at low temperatures. Several reports are available on the electrochemical studies of halide melts with CaO under  $\text{CO}_2$  flow.<sup>22,30</sup> But the mechanism is carbon dioxide reacted with CaO to form  $\text{CaCO}_3$ , which was further reduced as reaction (6). Therefore, this is not a direct  $\text{CO}_2$  splitting and will be discussed in the next section.

### 4. Electro-reduction of carbonates into nanocarbons

As discussed above, the direct splitting of  $\text{CO}_2$  could result in nanocarbons like CNTs, but lack of control. The products are mainly a collection of various carbon nanostructures. Moreover, it is difficult and dangerous in handling high pressure of  $\text{CO}_2$ . On the contrary, molten carbonates as storage materials of  $\text{CO}_2$  are easily handled and the reaction set-up could be much simple. Several groups recently reported the selective synthesis of nanocarbons by electro-reduction of molten carbonates with high yield. For example, our group successfully synthesized CNFs (carbon nanofibers)/CNTs from molten carbonate via a rational design inspired by chemical vapor deposition (CVD). The process is illustrated in Fig. 4.<sup>31</sup>

The CNTs were prepared by conducting the electrolysis between a 10  $\text{cm}^2$  coiled galvanized steel wire cathode (shown in Fig. 5)<sup>34</sup> and an oxygen generating nickel anode in 730 °C  $\text{Li}_2\text{CO}_3$  melt. The electrolysis was initiated at a low current of 5  $\text{mA/cm}^2$  on cathode, then constant current electrolysis at high current (100  $\text{mA/cm}^2$ ) for 2 to 4 Ah. As shown in Fig. 5, the solid carbon was deposited on the cathode, which proved to be carbon nanofibers (CNFs). The bright points presented in SEM are metal nucleation points for carbon fibers growth and was

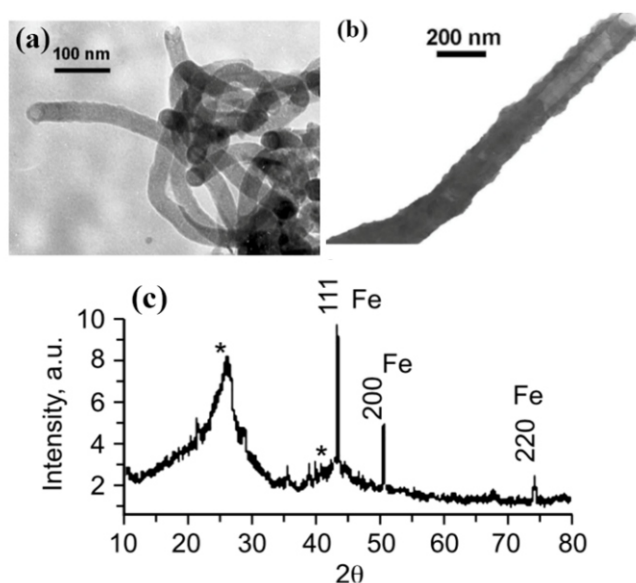
**Table 2** Standard potentials of electro-reductions of molten carbonates calculated from thermodynamic data. The thermodynamic data are from Ishan Barin, Thermochemical data of pure substances, 1995, VCH.

T/K	$E^{\circ}_{R3}/V$	$E^{\circ}_{R11}/V$	$E^{\circ}_{R9}/V$	$E^{\circ}_{R4a}/V$	$E^{\circ}_{R4b}/V$	$E^{\circ}_{R5a}/V$	$E^{\circ}_{R5b}/V$	$E^{\circ}_{R6}/V$	$E^{\circ}_{R8}/V$
298	-1.022	-1.333	-1.477	-2.360	-3.387	-2.403	-3.473	-2.040	-1.587
300	-1.022	-1.332	-1.476	-2.358	-3.385	-2.401	-3.470	-2.037	-1.586
400	-1.023	-1.287	-1.435	-2.262	-3.237	-2.301	-3.315	-1.915	-1.542
500	-1.023	-1.241	-1.395	-2.163	-3.086	-2.200	-3.159	-1.795	-1.499
600	-1.024	-1.195	-1.355	-2.066	-2.937	-2.100	-3.005	-1.676	-1.456
700	-1.024	-1.150	-1.316	-1.970	-2.791	-2.001	-2.853	-1.559	-1.413
800	-1.025	-1.104	-1.279	-1.876	-2.649	-1.904	-2.704	-1.443	-1.372
900	-1.025	-1.059	-1.242	-1.784	-2.509	-1.808	-2.557	-1.328	-1.330
1000	-1.026	-1.013	-1.208	-1.692	-2.371	-1.713	-2.413	-1.215	-1.289
1100	-1.026	-0.968	-1.185	-1.602	-2.236	-1.597	-2.225	-1.103	-1.250
1200	-1.026	-0.924	-1.163	-1.506	-2.088	-1.468	-2.012	-0.992	-1.215
1300	-1.026	-0.879	-1.142	-1.383	-1.887	-1.345	-1.812		-1.181
1400	-1.026	-0.834	-1.122	-1.261	-1.688	-1.225	-1.616		-1.148
1500	-1.027	-0.790	-1.102	-1.141	-1.492	-1.106	-1.423		

<sup>a</sup> Calculations based on graphite as the carbon product to calculate the above table.

<sup>b</sup> Standard potential of reaction (11)  $\text{CO}_2 \rightarrow \text{CO} + 1/2\text{O}_2$

$E^{\circ}_{RN}$  represents the standard potentials calculated by reaction N in the text. (N = 3,4a,4b, etc.)

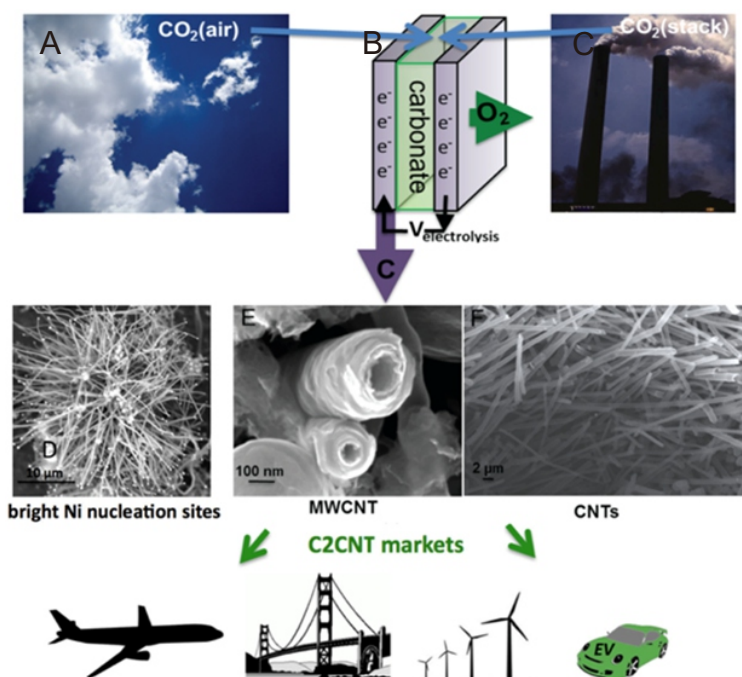


**Fig. 3** (a,b) TEM images of black powders produced in the system of NaCl-KCl- $\text{CO}_2$ , electrolysis conditions:  $P_{\text{CO}_2} = 1.0 \text{ MPa}$ ;  $T = 750^\circ\text{C}$ ;  $i_k = 13.5, 42 \text{ mA/cm}^2$ ; (c) XRD of products at  $i_k = 42 \text{ mA/cm}^2$ . Reprinted with permission from Ref. 66. Copyright 2008, Walter de Gruyter GmbH.

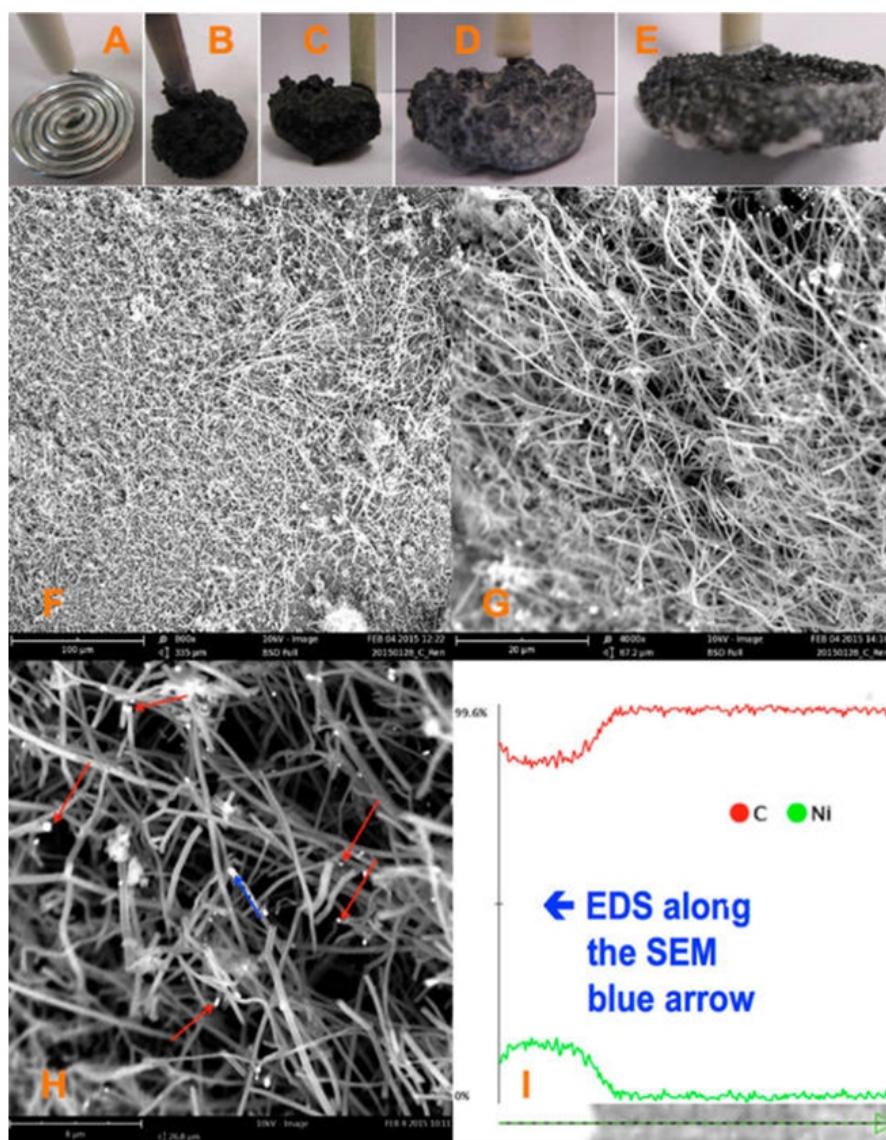


**Table 3** Electro-reductions standard potentials of some lithium salts contain atoms other than carbon. (Only indicating each reaction's tendency and possibility but giving no indication of the reaction's kinetics, such as rate and mechanism.)

T/K	$E^0$ ( $2\text{LiBO}_2 \rightarrow \text{Li}_2\text{O} + 2\text{B} + 3/2\text{O}_2$ )	$E^0$ ( $2\text{LiAlO}_2 \rightarrow \text{Li}_2\text{O} + 2\text{Al} + 3/2\text{O}_2$ )	$E^0$ ( $\text{Li}_2\text{SiO}_3 \rightarrow \text{Li}_2\text{O} + \text{Si} + \text{O}_2$ )	$E^0$ ( $\text{Li}_2\text{SO}_4 \rightarrow \text{Li}_2\text{O} + \text{S} + 3/2\text{O}_2$ )
298	-2.356	-2.920	-2.582	-1.312
300	-2.355	-2.919	-2.581	-1.311
400	-2.312	-2.868	-2.534	-1.266
500	-2.268	-2.817	-2.487	-1.219
600	-2.224	-2.766	-2.441	-1.172
700	-2.181	-2.715	-2.394	-1.126
800	-2.138	-2.665	-2.348	-1.080
900	-2.095	-2.614	-2.302	-1.036
1000	-2.052	-2.561	-2.255	-0.988
1100	-2.010	-2.507	-2.210	-0.940
1200	-1.978	-2.452	-2.164	-0.894
1300	-1.949	-2.398	-2.118	-0.849
1400	-1.921	-2.344	-2.072	
1500	-1.893	-2.289	-2.028	



**Fig. 4** Electrochemical synthesis of carbon nanostructures from  $\text{CO}_2$  in molten lithium carbonate. (D) SEM image of the carbon nanostructures with nickel as nucleation sites. (E) High magnification SEM of the synthesized carbon nanotubes and (F) Low magnification SEM of as-synthesized CNTs. Bottom: Carbon materials were applied in lightweight jets, strengthened bridges, wind turbines, and electric vehicle body components and batteries. Reprinted with permission from Ref. 31. Copyright 2017, Elsevier.



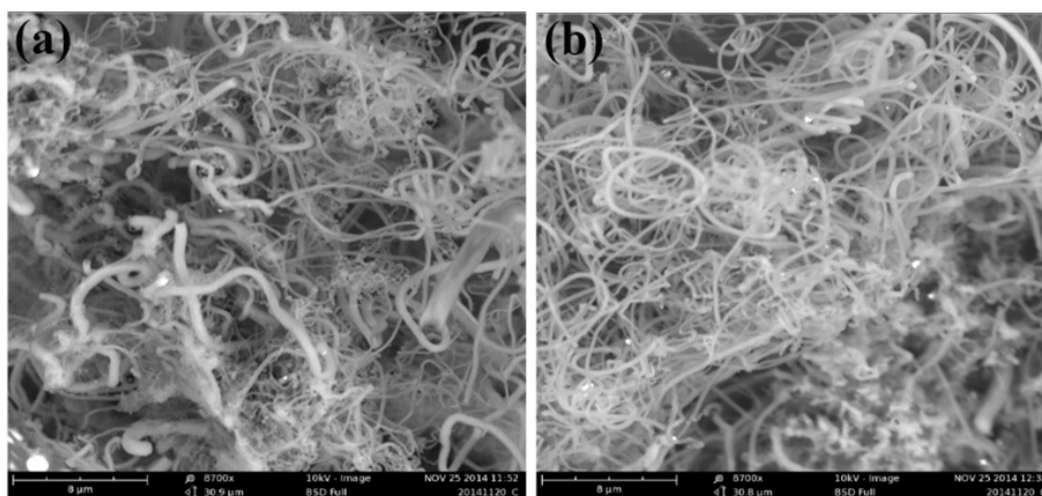
**Fig. 5** (A) A 10 cm<sup>2</sup> coiled galvanized steel wire cathode before electrolysis; (B–E) Typical cathodes after electrolysis in molten carbonate. (F–H) Various magnifications SEM of the product. Red arrows in SEM “H” indicate Ni nucleation sites. The blue arrow indicates moving track of Ni site along the CNF; (I) EDS mapping of the 6 µm blue arrow path shown in SEM “H”. Reprinted with permission from Ref. 34. Copyright 2015, American Chemical Society.

confirmed to be Ni by EDS measurement. The vast majority of the Ni nanoparticles in SEM are located at nanofiber tips, only a few seem to be aside from and not associated with CNF growth. The carbon fibers are homogeneous and have diameters of 200 to 300 nm, and length of 20 to 200 µm.

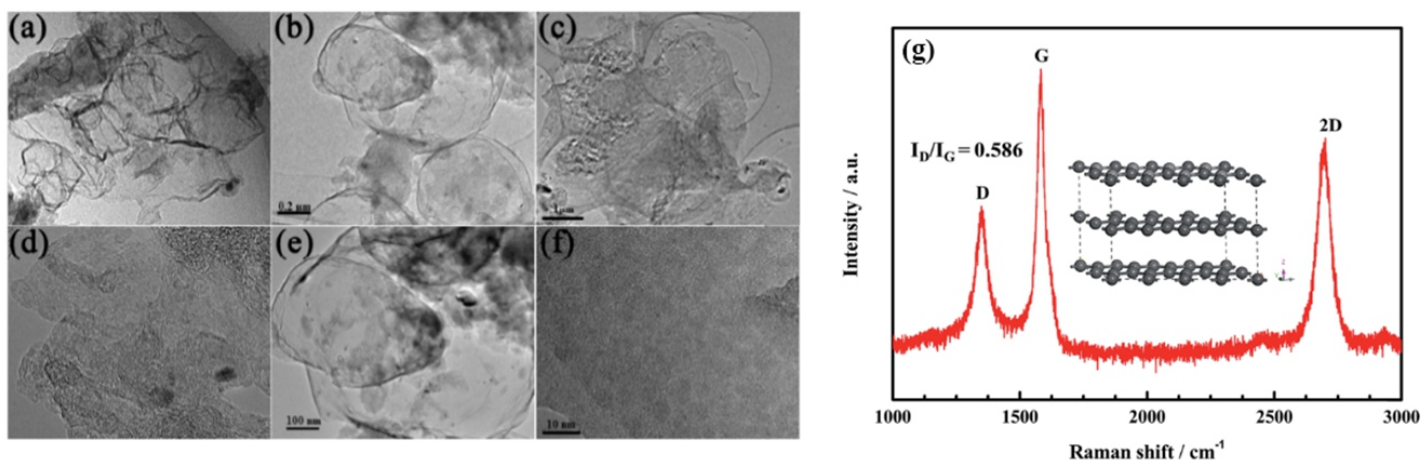
The linear EDS map in Fig. 5H shows Ni and C variation along the 6 µm path from pure Ni at the start of the fiber to pure carbon along the remainder of the fiber. The formation mechanism was proposed as: nickel (in this case originating from the Ni anode) first deposited on the cathode at initial low electrolysis currents (5 or 10 mA cm<sup>-2</sup>) because of its low reduction potential and low solubility. This is evidenced by the observed low electrolysis voltage (<0.7 V). The formation of nickel metals appears to be crucial to induce CNF formation. In Li<sub>2</sub>CO<sub>3</sub> melt, the electrolytic [CO<sub>3</sub><sup>2-</sup>] has much higher concentration and faster mass diffusion than that of [Ni<sup>2+</sup>], the carbonate reduction will be dominated

at high currents electrolysis. The higher electrolysis voltage thermodynamically required to deposit carbon is observed at current of >20 mA cm<sup>-2</sup>. Therefore, the initial low current nickel nucleation activation is necessary to form CNFs, instead, amorphous carbon will prefer to form. Interestingly, when Li<sub>2</sub>O was added to the molten Li<sub>2</sub>CO<sub>3</sub> electrolyte, tangled CNFs with a wide variety of diameters, instead of the straight/uniform diameter CNFs, were prepared as shown in Fig. 6. Consequently, the presence of high concentrations of oxide in Li<sub>2</sub>CO<sub>3</sub> electrolyte leads to the formation of tangled CNFs.

In addition to Ni, further studies demonstrate that Cu, Co and Fe can also act as nucleation sites in the synthesis of cathodic product of CNFs during electrolysis in molten carbonates. The nucleation metals for CNFs growth were required to have a lower reduction potential at low current density than that required for carbon deposition. The metals of nickel, copper, iron, and cobalt enhancing the production of CNFs by



**Fig. 6** SEM images of cathode product in 6M  $\text{Li}_2\text{O}/\text{Li}_2\text{CO}_3$  electrolyte. Reprinted with permission from Ref. 34. Copyright 2015, American Chemical Society.



**Fig. 7** TEM images of the products obtained on (a) stainless steel, (b) Cu, and (c) Ni electrode at 750 °C in  $\text{CaCl}_2\text{--NaCl--CaO}$ . HRTEM images of the product obtained on (d) stainless steel, (e) Cu, and (f) Ni electrode. Reprinted with permission from ref. 35. Copyright 2016, John Wiley & Sons, Inc. (g) Raman spectroscopy of obtained material. Reprinted with permission from Ref. 22. Copyright 2015, Royal Society of Chemistry.

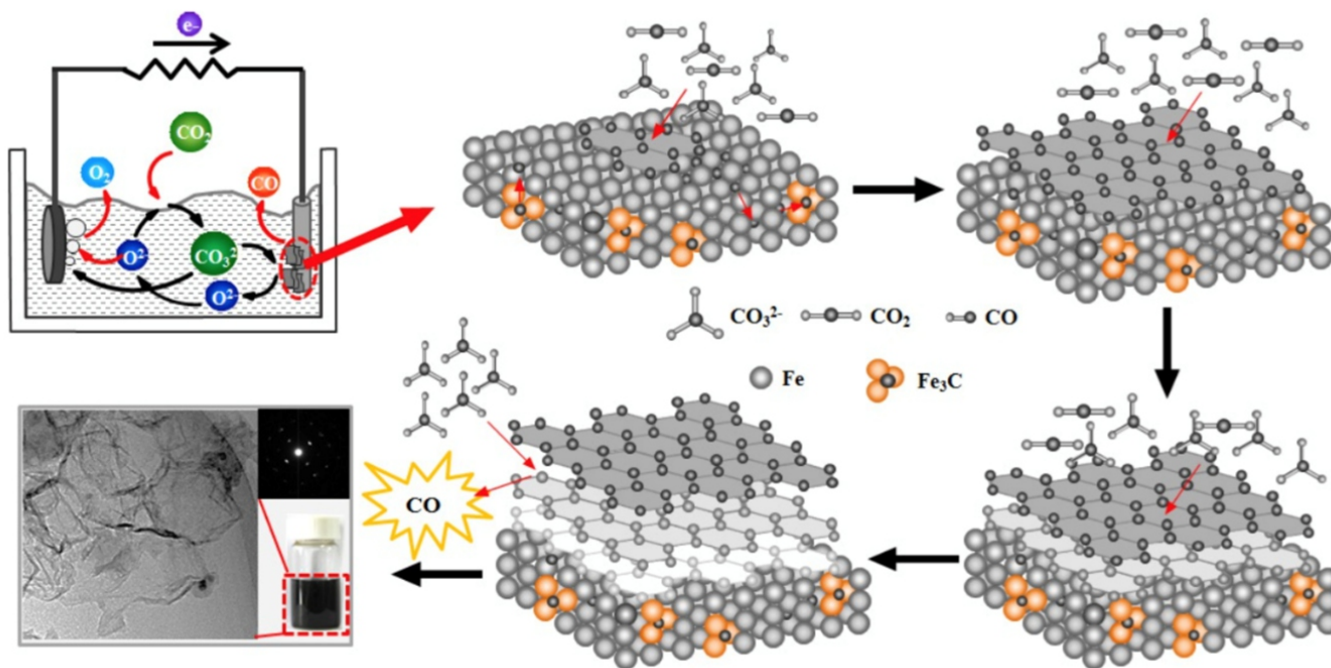
molten electrolysis are also used as catalysts for CVD growth of CNFs.<sup>69–71</sup> Ni, Co, Cu or Fe was deposited at low current density from electrolytes which have a low concentration of the metal, and dissolved as oxide. The deposition of these nucleation sites on the cathode promote the CNFs formation and growth. In contrast, a solid metal cathode does not exhibit these characteristics and no homogeneous CNFs were formed. In the case of pure iron metal cathode, an overabundance of Fe results in uncontrolled carbon deposition and growth, which leads to the formation of randomly distributed (amorphous) carbon. Our group's results were further explored by other groups to control the diameter and length by means of tuning reaction time and catalyst particle size.<sup>33,72–75</sup>

Besides CNTs/CNFs, the efforts have also been made on the syntheses of graphene-like materials. Hu and co-workers systematically investigated the electrochemical reactions in a  $\text{CaCl}_2\text{--CaO}$  or  $\text{CaCl}_2\text{--NaCl--CaO}$  melt under  $\text{CO}_2$  flow.<sup>20,30,35</sup> The anode is  $\text{RuO}_2\cdot\text{TiO}_2$  and

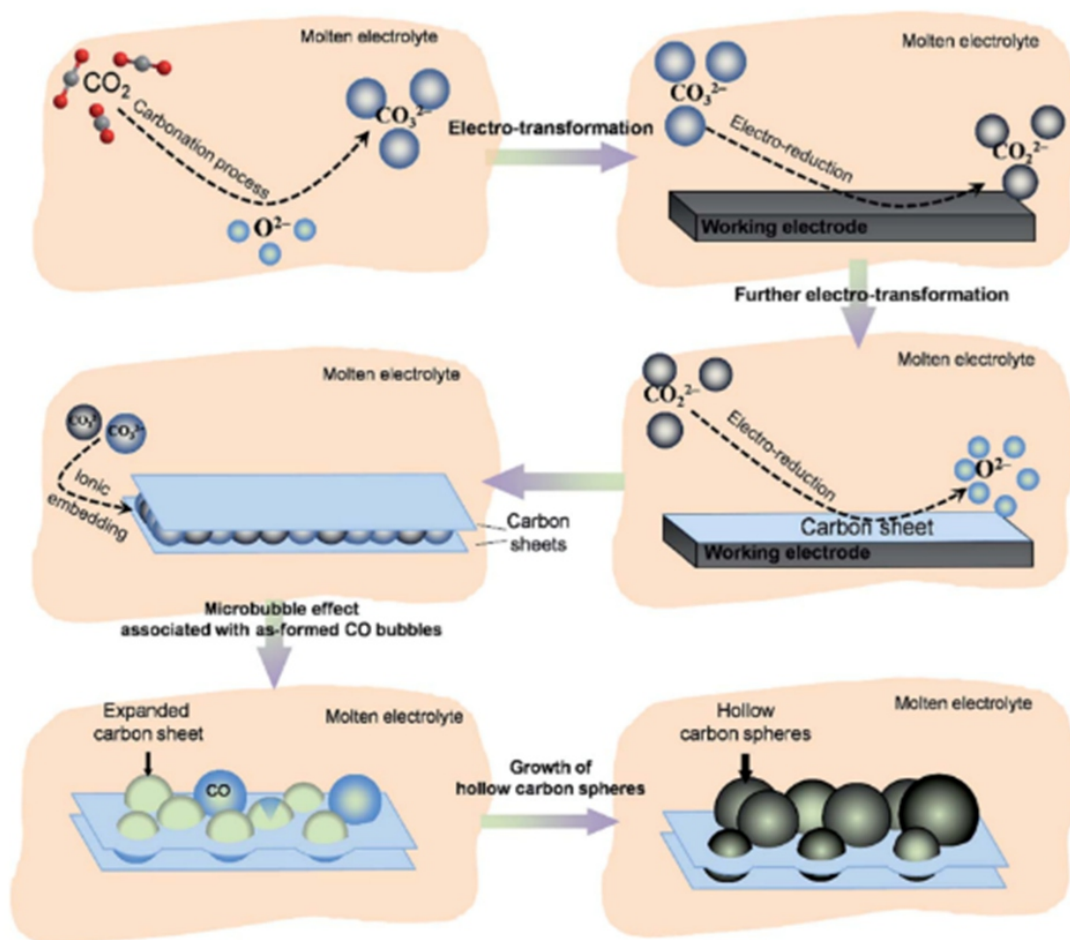
various metals, including tungsten wire, Cu, stainless steel, Ni, were employed as the cathode. In both cases, a few layers of graphene could be produced as evidenced by TEM and Raman.<sup>22,35</sup>

The results showed that this process was temperature- and cathode-dependent. The carbon deposited at the stainless steel cathode at 750 °C (Fig. 7 a, d) has a “wrinkled sheet” structure that resembles graphene, while thick graphite flake and flat sheet with fewer layers were obtained at 650 °C and 850 °C, respectively. The product obtained on the Cu rod at 750 °C displays a special graphene ball structure with rolled edges (Fig. 7b, e). When Ni was used as a cathode, a flat-shaped graphene sheet with a few layers was observed (Fig. 7e, f). The results state clearly that the graphene structure is affected by the catalysis of metal atoms at the cathode. The mechanism was proposed to be metal-catalyzed deposition and micro-explosion of CO, as shown in Fig. 8. It should be noted if glassy carbon was employed as cathode, CNTs could be synthesized in  $\text{CaCl}_2\text{--NaCl--CaO}$  melt.<sup>35</sup>





**Fig. 8** The electrochemical synthesis of graphene on stainless steel cathode in molten  $\text{CaCl}_2\text{-NaCl-CaO}$ . Reprinted with permission from Ref. 35. Copyright 2016, John Wiley & Sons, Inc.



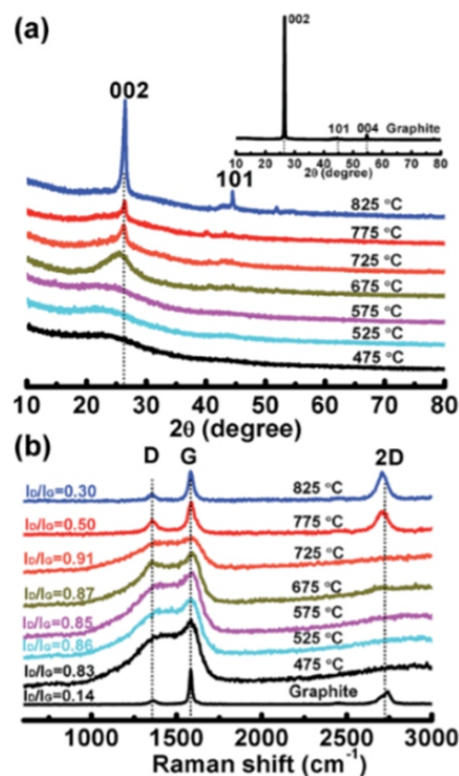
**Fig. 9** Mechanism of the formation of hollow spheres. Reprinted with permission from Ref. 40. Copyright 2017, Royal Society of Chemistry.

In addition to CNTs and graphene, other types of carbon structures were also successfully produced via electro-reduction of  $\text{CO}_2$ . Typically, spherical, flake, random-shaped carbons were obtained. But some interesting materials were also obtained via this route. One-step high-yield synthesis of hollow carbon spheres by electrochemical reduction of  $\text{CO}_2$  in a  $\text{CaCO}_3$ - $\text{LiCl}$ - $\text{KCl}$  melt at  $450^\circ\text{C}$  was reported by Wang *et al.*<sup>40</sup> The formation mechanism was proposed as displayed in Fig. 9, by the following processes (1) formation of  $\text{CO}_3^{2-}$  via  $\text{CO}_2$  absorption; (2)  $\text{CO}_3^{2-}$  was reduced to  $\text{CO}_2^{2-}$ ; (3)  $\text{CO}_2^{2-}$  was further reduced to carbon and carbon sheets were deposited on the cathode during electrolysis; (4) remaining unreacted  $\text{CO}_2^{2-}$  or  $\text{CO}_3^{2-}$  was encapsulated into the carbon sheets and further reduced to CO; (5) the growing CO bubbles expand the carbon sheets to bubble-like structures; and (6) CO bubbles were further reduced to solid carbon and form hollow carbon sphere. It is worthwhile to note that growth of hollow carbon spheres deeply relies on the electrolyte composition and the precise control of electrode potential. The  $\text{CaCO}_3$  in the melt ( $\text{LiCl}$ - $\text{KCl}$ - $\text{CaCO}_3$ ) accounts for the release of CO and the resulting microbubble effect. If  $\text{Li}_2\text{CO}_3$  was present instead of  $\text{CaCO}_3$ , CO was not found during electrolysis under temperature below  $850^\circ\text{C}$  and the current of carbonate reduction in  $\text{LiCl}$ - $\text{KCl}$ - $\text{Li}_2\text{CO}_3$  was much higher than that in  $\text{LiCl}$ - $\text{KCl}$ - $\text{CaCO}_3$ , which lead to the carbon products aggregating to form carbon nanoparticles instead of carbon hollow spheres. During the electrolysis in  $\text{LiCl}$ - $\text{KCl}$ - $\text{Li}_2\text{CO}_3$ , the fast conversion of  $\text{CO}_3^{2-}$  to C prevents the accumulation of unreacted  $\text{CO}_2^{2-}$ , thus, the reduction of  $\text{CO}_2^{2-}$  to carbon sheets and its subsequent microbubble effect would not occur.<sup>40</sup>

Nanostructured graphite was also prepared by the same group via the electrochemical reduction of molten  $\text{Li}_2\text{CO}_3$ - $\text{Na}_2\text{CO}_3$ - $\text{K}_2\text{CO}_3$ - $\text{Li}_2\text{SO}_4$  under synthetic flue gas flow (a mixture of  $\text{CO}_2$  and  $\text{SO}_2$ ) at a relatively low temperature of  $775^\circ\text{C}$ .<sup>71</sup> The mechanism is relative complicated, but it is certain that this process is temperature dependent and without  $\text{Li}_2\text{SO}_4$  in the liquid electrolyte and  $\text{SO}_2$  in the gas, the graphitization could not happen. As proposed by the authors, the electro-reduction of sulfate ions to  $\text{S}^{2-}$  and S plays important role to de-oxygenate, and the in-situ  $\text{SO}_2$  adsorption to form sulfate ions made this process to be a cycle. Sulfur can react with defective carbon in the matrix to form  $\text{CS}_2$  resulting in the removal of imperfect carbons, and thus leads to a high degree of graphitization. Meanwhile, the  $\text{S}^{2-}$  ions facilitates the deoxygenation of graphite via reaction  $\text{S} + 2[\text{O}] \rightarrow \text{SO}_2$ .<sup>71</sup> Therefore, sulfur assisted oxygen and defect carbon removal are favorable for the

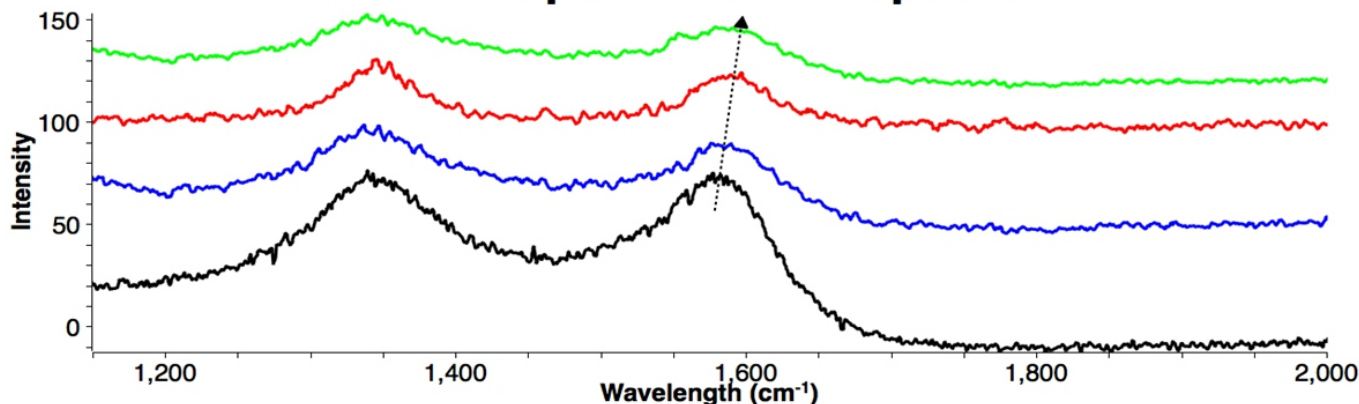
formation of high degree crystallize graphite on the cathode at a temperature of  $775^\circ\text{C}$ .

Doped carbon materials exhibited enhanced properties, i.e. B-doped carbon for enhanced conductivity, N-doped carbon for high performance supercapacitor and excellent electro-catalytic activity, S-doped carbon for the heavy metal ion removal, etc.<sup>31,76-78</sup> The possibility of preparation of doped CNTs from  $\text{CO}_2$  was explored by Ren *et al.* with the examples of B-, S-, and P-doped carbons by using  $\text{Li}_2\text{CO}_3$  as



**Fig. 10** (a) XRD and (b) Raman spectra of the commercial graphite and the electrolytic carbon materials obtained at different temperatures. Reprinted with permission from Ref. 71. Copyright 2017, Royal Society of Chemistry.

## Raman Spectra of B-doped CNTs



**Fig. 11** Raman spectra of B-doped CNTs obtained from different  $\text{LiBO}_2$  addition in  $50\text{g}$   $\text{Li}_2\text{CO}_3$ , from bottom to top the addition is 1.5g, 3g, 5g and 8g, respectively. Reprinted with permission from Ref. 31. Copyright 2017, Elsevier.

the electrolyte plus certain amount of  $\text{LiBO}_2$  (Raman spectroscopy of B-doped CNTs in Fig. 11),  $\text{Li}_2\text{SO}_4$  or  $\text{LiPO}_3$ .<sup>31,79</sup> The presence of B-, S-, and P-atom was confirmed by element analysis and Raman spectroscopy. However, their performances in adsorption, catalysis, etc., are still unknown.

## 5. Applications

Carbon materials are unique in energy storage because of their high surface area, excellent conductivity, strong resistance to acid/base/organic solvents, and tailorable crystal structures. The electrolytic carbons from  $\text{CO}_2$  were tested in batteries and supercapacitors and displayed enhanced performances. The carbon materials prepared by electrochemical reduction of  $\text{CO}_2$  in Li-Na-K carbonate melts were used as negative electrode materials for Li-ion batteries. A high reversible capacity of  $798 \text{ mAh g}^{-1}$  at  $50 \text{ mA g}^{-1}$ , which is more than two times higher than the theoretical capacity of graphite was achieved and it retains at  $266 \text{ mAh g}^{-1}$  over 500 cycles at a current density up to  $500 \text{ mA g}^{-1}$ .<sup>80</sup> Licht and co-workers also reported the results of electrolytic CNTs (straight and tangled) from  $\text{CO}_2$  as the anode material in Lithium-ion and Sodium-ion batteries. Both straight (from pure  $\text{Li}_2\text{CO}_3$  electrolyte) and tangled CNTs (from  $\text{Li}_2\text{O}/\text{Li}_2\text{CO}_3$  electrolyte) displayed similar capacity of  $\sim 350 \text{ mAh g}^{-1}$  in the initial 15 cycles in Li-ion battery test. After 200 cycles, the tangled CNT capacity increase to  $\sim 460 \text{ mAh g}^{-1}$ , while the capacity of straight CNTs remains at  $\sim 360 \text{ mAh g}^{-1}$ .<sup>53</sup> Such increased capacity during cycling has been reported in previous studies on carbon nanostructured electrodes, indicating the effect of the defect-induced modification to storage processes during cycling, particularly, with very high defect-containing carbons.<sup>81</sup> Based on the comparison of straight CNTs ( $I_D/I_G$  is 0.4 from Raman spectra) with tangled CNTs ( $I_D/I_G$  is 0.9 from Raman spectra), the high degree defects and bend in the tangled CNTs enable a transition from dilute staging of  $\text{Li}^+$ , which occurs during the formation of  $\text{LiC}_{6n}$ , to a combination of this and the so called “intercalation and pore-filling” mechanism at defect sites.<sup>81</sup> The continuous activation of this storage mode enables a capacity superior to the maximum alloying capacity of Li in  $\text{LiC}_6$ .

However, in sodium-ion battery test, the charge-discharge behaviors are quite different between straight and tangled CNTs. The reversible capacity of the straight CNTs is only slightly higher than the maximum intercalation capacity of  $\text{Na}^+$  in pure graphite. But the tangled CNTs show reversible capacities over  $130 \text{ mAh g}^{-1}$ , about two times higher than that of the straight CNTs. The results suggest that defects in CNTs (the tangled CNTs synthesized from the STEP process) are crucial to trigger the  $\text{Na}^+$  storage. The in-situ adsorption and electrochemical reduction of  $\text{CO}_2$  with STEP process provide a promising technology to develop high-performance carbon negative electrode materials for Li-ion batteries.<sup>53</sup>

When applying in supercapacitors, the capacitances of these electrolytic carbons in most reports are below  $200 \text{ F/g}$ . A very interesting report from Wang's group is sulfur-doped carbons prepared from the electrochemical reduction of molten  $\text{Li}_2\text{CO}_3\text{--Na}_2\text{CO}_3\text{--K}_2\text{CO}_3\text{--Li}_2\text{SO}_4$  at  $475^\circ\text{C}$  by using nickel and  $\text{SnO}_2$  as the cathode and anode respectively.<sup>48</sup> The S-doped carbons exhibit high surface-area-normalized capacitance of  $71.5 \mu\text{F cm}^{-2}$ , high gravimetric capacitance of  $257.3 \text{ F g}^{-1}$  and excellent cycling stability. This continuous-operation process is promising for massive preparation of advanced carbon materials for energy applications by the integration of carbon reduction and deep desulfurization from practical waste gas without purification. Additionally, carbons from  $\text{CO}_2$  have been tested in other applications as well, such as the oxygen reduction and adsorption material for aqueous pollutants  $\text{Cu(II)}$  ion and methylene blue (MB).<sup>82,83</sup>

However, it is only in an early stage of the investigation of electrolytic carbons. Many possibilities may happen since this method can create carbons with controlled hetero-atom doping, controlled morphology, and high surface area.

## 6. Conclusion and future perspectives

As evidenced by latest studies, molten salts could be employed for better graphitization,<sup>39</sup> and create new materials by in-situ insertion of graphite. Electrochemical interaction between graphite and molten salts enables the preparation of carbon nanotubes, nanoparticles, graphene and nanodiamonds in molten salts. Electro-reduction of  $\text{CO}_2$ , either direct or indirect vs carbonate is versatile and powerful approach to create functional materials in a diversity of applications. More efforts should be made in (1) the defects control of electrolytic carbons, which is very important as electro-active materials, (2) detecting possibility of synthesis of SWCNTs or DWCNTs, fullerenes, Single layer or double layer graphene, etc., and (3) hetero-atom doped carbons.

## Conflict of interest

There are no conflicts to declare.

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